

This Page Is Inserted by IFW Operations
and is not a part of the Official Record

BEST AVAILABLE IMAGES

Defective images within this document are accurate representations of the original documents submitted by the applicant.

Defects in the images may include (but are not limited to):

- BLACK BORDERS
- TEXT CUT OFF AT TOP, BOTTOM OR SIDES
- FADED TEXT
- ILLEGIBLE TEXT
- SKEWED/SLANTED IMAGES
- COLORED PHOTOS
-  BLACK OR VERY BLACK AND WHITE DARK PHOTOS
- GRAY SCALE DOCUMENTS

IMAGES ARE BEST AVAILABLE COPY.

**As rescanning documents *will not* correct images,
please do not report the images to the
Image Problem Mailbox.**

PCT

WORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

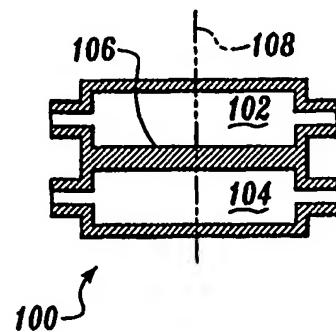
(51) International Patent Classification 7 : B01J 8/02, C01B 3/38, 3/16, B01J 12/00	A1	(11) International Publication Number: WO 00/06295 (43) International Publication Date: 10 February 2000 (10.02.00)
---	----	---

(21) International Application Number: PCT/US99/17084 (22) International Filing Date: 27 July 1999 (27.07.99) (30) Priority Data: 09/123,779 27 July 1998 (27.07.98) US	(81) Designated States: CA, JP, MX, NO, European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE). Published <i>With international search report.</i>
(71) Applicant: BATTELLE MEMORIAL INSTITUTE [US/US]; Pacific Northwest Division, Intellectual Property Services, P.O. Box 999, Richland, WA 99352 (US). (72) Inventors: TONKOVICH, Anna, Lee, Y.; 1604 37th Place North, Pasco, WA 99301 (US). WANG, Yong; 2884 Troon Court, Richland, WA 99352 (US). WEGENG, Robert, S.; 2603 Harris, Richland, WA 99352 (US). GAO, Yufei; 302 North Hawaii, Kennewick, WA 99336 (US). (74) Agent: ZIMMERMAN, Paul, W.; Battelle Memorial Institute, Pacific Northwest Division, Intellectual Property Services, P.O. Box 999, MSIN: K1-53, Richland, WA 99352 (US).	

(54) Title: METHOD AND APPARATUS FOR OBTAINING ENHANCED PRODUCTION RATE OF THERMAL CHEMICAL REACTIONS

(57) Abstract

The present invention is a method and apparatus (vessel) for providing a heat transfer rate from a reaction chamber through a wall to a heat transfer chamber substantially matching a local heat transfer rate of a catalytic thermal chemical reaction. The key to the invention is a thermal distance defined on a cross-sectional plane through the vessel inclusive of a heat transfer chamber, reaction chamber and a wall between the chambers. The cross-sectional plane is perpendicular to a bulk flow direction of the reactant stream, and the thermal distance is a distance between a coolest position and a hottest position on the cross-sectional plane. The thermal distance is of a length wherein the heat transfer rate from the reaction chamber to the heat transfer chamber substantially matches the local heat transfer rate.



FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AL	Albania	ES	Spain	LS	Lesotho	SI	Slovenia
AM	Armenia	FI	Finland	LT	Lithuania	SK	Slovakia
AT	Austria	FR	France	LU	Luxembourg	SN	Senegal
AU	Australia	GA	Gabon	LV	Latvia	SZ	Swaziland
AZ	Azerbaijan	GB	United Kingdom	MC	Monaco	TD	Chad
BA	Bosnia and Herzegovina	GE	Georgia	MD	Republic of Moldova	TG	Togo
BB	Barbados	GH	Ghana	MG	Madagascar	TJ	Tajikistan
BE	Belgium	GN	Guinea	MK	The former Yugoslav Republic of Macedonia	TM	Turkmenistan
BF	Burkina Faso	GR	Greece			TR	Turkey
BG	Bulgaria	HU	Hungary	ML	Mali	TT	Trinidad and Tobago
BJ	Benin	IE	Ireland	MN	Mongolia	UA	Ukraine
BR	Brazil	IL	Israel	MR	Mauritania	UG	Uganda
BY	Belarus	IS	Iceland	MW	Malawi	US	United States of America
CA	Canada	IT	Italy	MX	Mexico	UZ	Uzbekistan
CF	Central African Republic	JP	Japan	NE	Niger	VN	Viet Nam
CG	Congo	KE	Kenya	NL	Netherlands	YU	Yugoslavia
CH	Switzerland	KG	Kyrgyzstan	NO	Norway	ZW	Zimbabwe
CI	Côte d'Ivoire	KP	Democratic People's Republic of Korea	NZ	New Zealand		
CM	Cameroon			PL	Poland		
CN	China	KR	Republic of Korea	PT	Portugal		
CU	Cuba	KZ	Kazakhstan	RO	Romania		
CZ	Czech Republic	LC	Saint Lucia	RU	Russian Federation		
DE	Germany	LI	Liechtenstein	SD	Sudan		
DK	Denmark	LK	Sri Lanka	SE	Sweden		
EE	Estonia	LR	Liberia	SG	Singapore		

METHOD AND APPARATUS FOR OBTAINING ENHANCED PRODUCTION RATE OF THERMAL CHEMICAL REACTIONS

5

FIELD OF THE INVENTION

The present invention relates to a method and apparatus for thermal
10 chemical reactions. More specifically, the method and apparatus provide an enhanced reaction rate for the thermal chemical reaction.

As used herein, the term thermal chemical reaction(s) includes exothermic and endothermic chemical reactions.

15

BACKGROUND OF THE INVENTION

Thermal chemical reactions including exothermic and endothermic chemical reactions are well known. Examples of thermal chemical reactions include but are not limited to Hydrogen and Hydrocarbon conversion reactions
20 including but not limited to steam reforming, water-gas shift reactions and combustion are well known. These reactions are usually carried out in the presence of a catalyst at temperatures up to about 1000 °C . Because the intrinsic kinetics of the thermal chemical reaction are much faster than the heat transfer rate between the reaction vessel and the thermal sink or environment,
25 the rate of product production is limited. Limited production rates may be characterized in terms of residence time which is typically seconds to minutes in convention thermal chemical reaction vessels.

For example, the water gas shift reaction is conventionally carried out in fixed bed reactors. The water gas shift reaction of converting carbon monoxide
30 and water to carbon dioxide and hydrogen suffers from multiple-second residence times (kinetic impediment) when carried out in fixed bed reactors. Theoretical kinetics suggests possible residence times on the order of milliseconds. There are two kinetic retarding aspects to conventional reactors. The first is a diffusion limitation as reactants diffuse into and out of a catalyst bearing porous pellet and the second is a heat transfer limitation which is a
35

combination of heat transfer parameters (conduction, length) of catalyst supports and overall reactor geometry (shape and size). Because the water gas shift reaction is critical to a multi-reactor fuel processing system that supports distributed energy production through the use of a fuel cell, there is a need for a 5 smaller, faster water gas shift reactor.

Another example is conventional methane steam reforming reactor produces synthesis gas at an average residence time of several seconds and with an effectiveness factor of 0.01 to 0.05 reported by Adris, A., Pruden, B., Lim, C., J. Grace, 1996, On the reported attempts to radically improve the performance of 10 the steam methane reforming reactor, Canadian Journal of Chemical Engineering, 74, 177-186. In typical industrial operation, the methane to steam ratio is run at 3:1 to prevent coke formation.

Efforts to improve heat transfer between the reaction vessel and the thermal sink have made only modest improvements in product production rate. 15 Thus, there is a need in the art of thermal chemical reactions for a method and apparatus that increases the heat transfer rate between the reaction vessel and the thermal sink and thereby approach the theoretical intrinsic kinetic rate of reaction and production.

20 SUMMARY OF THE INVENTION

The present invention is a method and apparatus for obtaining an enhanced production rate per reaction chamber volume of a reaction chamber with an inlet and an outlet for a thermal chemical reaction, wherein a ratio of the 25 enhanced production rate per reaction chamber volume to a conventional production rate per conventional reaction chamber volume for the thermal chemical reaction is at least 2. For example, for convention steam reforming residence time is on the order of seconds whereas with the present invention, residence time is less than a factor of 2, on the order of milliseconds. The 30 method and apparatus rely upon;

(a) a porous insert within the reaction chamber volume, wherein a reactant flow substantially completely passes through the porous insert

wherein the reaction chamber volume with the porous insert has a mean porosity less than 1 and a transport distance no greater than 3 mm;

- (b) the reaction chamber volume with a length parallel to a bulk reactant flow, the length less than or equal to 6 inches, and with a height less than or equal to 2 inches, thereby transferring reaction heat at an enhanced heat transfer rate through the porous insert; and
- (c) a heat transfer chamber in thermal contact with the reaction chamber volume, the heat transfer chamber transferring heat at said enhanced heat transfer rate across a wall between the heat transfer chamber and the reaction chamber, thereby obtaining the enhanced production rate per reaction chamber volume for the thermal chemical reaction wherein a ratio of the enhanced production rate per reaction chamber volume to a conventional production rate per conventional reaction chamber volume for the thermal chemical reaction is at least 2.

These features have been found to cooperate with the reaction kinetics in terms of transferring heat at a rate sufficient to avoid substantial impediment of the kinetics. These features are effective for both catalytic and non-catalytic thermal chemical reactions. For catalytic chemical reactions, addition of a catalyst upon the porous insert permits flow of reactants past catalyst sites rather than limiting reactant motion to diffusion as in conventional systems. Thus, according to the present invention, for catalytic thermal chemical reactions, both kinetic impediments are substantially reduced permitting realization of theoretical or near theoretical reaction kinetics. More specifically, a water gas shift reactor made according to the present invention has 1/10th to 1/100th the size of conventional processing hardware for the same production output.

The subject matter of the present invention is particularly pointed out and distinctly claimed in the concluding portion of this specification. However, both the organization and method of operation, together with further advantages and objects thereof, may best be understood by reference to the following description taken in connection with accompanying drawings wherein like reference characters refer to like elements.

BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1a is a cross section of a stacked reaction chamber with heat
5 exchanger chamber.

FIG. 1b is an isometric of a nested reaction chamber with heat exchanger
chamber.

FIG. 2a is a graph of percent selectivity versus residence time for long
contact time water gas shift with a powder catalytic porous insert.

10 FIG. 2b is a graph of percent selectivity versus residence time for short
contact time water gas shift with a powder catalytic porous insert.

FIG. 3 is a graph of percent selectivity versus temperature for various
residence times for water gas shift with a coated metal foam porous insert.

15 FIG. 4 is a graph of methane conversion versus temperature for various
residence times for a steam to methane ratio of 2.5:1.

FIG. 5a is a graph of conversion and selectivity versus time for n-butane
steam reforming with a porous insert of a porous substrate with interfacial layer
and catalyst material.

20 FIG. 5b is a graph of conversion and selectivity versus time for n-butane
steam reforming with a regenerated porous insert.

DESCRIPTION OF THE PREFERRED EMBODIMENT(S)

25 Referring to FIG. 's 1a and 1b, a vessel 100 for thermal chemical
reactions the vessel having two chambers 102 and 104 with a wall 106
therebetween. Either of the two chambers 102, 104 may be the reaction
chamber. Bulk flow of reactants within the reaction chamber 102 is substantially
30 perpendicular to a cross section plane 108. The vessel 100 may have stacked
chambers as in FIG. 1a or nested chambers as in FIG. 1b. The reaction in the
reaction chamber may be endothermic or exothermic.

In a thermal chemical reaction, the rate of production (reaction kinetics) is
limited by the rate of heat transfer either to (endothermic) or from (exothermic)
the reaction site. In order to obtain an enhanced heat transfer rate and thereby
35 an enhanced production rate, the reaction chamber has a porous insert (not

shown) within the reaction chamber volume wherein the reaction chamber volume with the porous insert has a mean porosity less than 1 and a transport distance no greater than 3 mm, thereby transferring reaction heat at an enhanced heat transfer rate through the porous insert.

5 The porous insert may be a powder, a porous monolith (including but not limited to metal or ceramic foam, honeycomb, tube bank, stacked microchannel assembly, and combinations thereof), fibers (e.g. steel wool), or combinations thereof. In view of the cost of replacing spent catalyst, for catalytic reactors, it is preferred that the porous insert be removable from the reaction chamber. The
10 porous insert may be arranged to provide single or multiple flow passages for reactants through the reaction chamber volume. The porous insert may rest on or contact raised features formed on the interior surface(s) of the reaction chamber.

For catalytic thermal chemical reactions, a preferred porous insert is a
15 porous support with a catalyst material thereon. More preferred is a porous insert with a solution deposited interfacial layer between the porous support and the catalyst material. A more preferred porous insert has a buffer layer between the porous support and the interfacial layer.

In addition, the reaction chamber volume has a length parallel to a bulk
20 reactant flow, the length less than or equal to 6 inches, and has a height less than or equal to 2 inches. The limited length and height provide short distances for the projections thereby permitting faster heat transfer. Moreover, the short length reduces overall pressure drop through the reaction chamber.

The heat transfer chamber is in thermal contact with the reaction chamber
25 volume, the heat transfer chamber transferring heat at the enhanced heat transfer rate across the wall 106 between the heat transfer chamber and the reaction chamber, thereby obtaining the enhanced production rate per reaction chamber volume for the thermal chemical reaction.

The interfacial layer is a solution deposited metal oxide. The solution
30 deposited metal oxide includes but is not limited to $\gamma\text{Al}_2\text{O}_3$, SiO_2 , ZrO_2 , TiO_2 , magnesium oxide, vanadium oxide, chromium oxide, manganese oxide, iron oxide, nickel oxide, cobalt oxide, copper oxide, zinc oxide, molybdenum oxide, tin oxide, calcium oxide, aluminum oxide, lanthanum series oxide(s), zeolite(s)

and combinations thereof. Typically the porous support has a thermal coefficient of expansion different from that of the interfacial layer. Accordingly, for high temperature catalysis ($T > 150^{\circ}\text{C}$) a buffer layer is needed to transition between the two coefficients of thermal expansion.

5 The buffer layer is a metal oxide that is Al_2O_3 , TiO_2 and combinations thereof. More specifically, the Al_2O_3 is α - Al_2O_3 , γ - Al_2O_3 and combinations thereof. The structure of the α - Al_2O_3 is preferred because TiO_2 is not as a good material as alumina against oxygen diffusion. Therefore, it is expected that resistance against high temperature oxidation can be improved with alumina coated foam. When the porous substrate 100 is metal foam, a preferred embodiment has a buffer layer formed of two sub-layers. The first sublayer is α - Al_2O_3 for passivating the metal foam and the second layer is TiO_2 for bonding to the interfacial layer.

10 Deposition of the buffer layer 102 may be by vapor deposition including but not limited to chemical vapor deposition, physical vapor deposition or combinations thereof. Because the vapor deposition is conducted at high temperatures, polycrystalline phases are formed providing good adhesion of the metal oxide to the metal foam surface.

15 Alternatively, the buffer layer 102 may be obtained by solution coating. The solution coating has the steps of metal surface functionalization via hydroxide formation, followed by surface hydrolysis of alkoxides to obtain the polycrystalline phases. This solution coating may be preferred as a lower cost method of depositing the buffer layer 102.

20 Polycrystalline metal oxides resist flaking off under thermal cyclings. The open cells of a metal foam may range from about 20 ppi to about 1000 ppi and is preferably about 80 ppi.

25 The catalyst material (when used) is deposited onto the interfacial layer. The catalyst material may be any catalyst metal including but not limited to noble metal, transition metal and combinations thereof, or a catalyst metal oxide or transition metal oxide including but not limited to magnesium oxide, titanium oxide, vanadium oxide, chromium oxide, manganese oxide, iron oxide, nickel oxide, cobalt oxide, copper oxide, zinc oxide, zirconium oxide, molybdenum

oxide, tin oxide, calcium oxide, aluminum oxide, silicon oxide, lanthanum series oxide(s), zeolite(s) and combinations thereof.

The method of making the preferred catalyst has the steps of selecting a porous support, vapor depositing a buffer layer on the porous support, solution 5 depositing a interfacial layer thereon, and depositing a catalyst metal onto the interfacial layer. When a metal foam is used as the porous support, the metal foam is etched prior to vapor depositing the buffer layer. Etching is preferably with an acid, for example HCl. Optionally a catalyst layer may be deposited onto the interfacial layer.

10

Example 1

An experiment was conducted to demonstrate a chemical thermal reactor according to the present invention using the water gas shift reaction.

A first porous insert was made with a catalyst material of a pre-reduced and 15 stabilized 5-wt% Ru/ZrO₂ catalyst (1/8-inch extrudates) obtained from Degussa Corporation. The catalyst material was ground and sieved to 65 to 100 mesh.

A second porous insert was made with Ni metal foam with 80 pores per inch (ppi) machined to fit in a 7 mm ID quartz tube, ranging from 0.5 to 2.5 cm in length. The metal foam was washed in a sonicator with acetone, chloroform, 20 and water successively over 10-minute intervals. It was also etched in a 1M HCl solution at 60 °C for 30 min. The etched metal foam was saturated with a zirconium n-propoxide/1-propanol solution (Aldrich), followed by ambient hydrolysis with water vapor for 72 h, then calcined at 450 °C for 4 h to form the interfacial layer. The ZrO₂ -coated metal foam was saturated with a dilute aqueous RuCl₃ solution (RuCl₃ hydrate, Aldrich). The saturation process was 25 repeated several times until the desired Ru loading was achieved. The coated metal foam supported Ru catalyst was finally dried at 100 °C in vacuum overnight, followed by calcination at 350 °C for 1 h. Prior to testing, the catalyst was activated with a 10%H₂/He mixture at 350 °C for at least 1 h.

30 A catalytic plug flow reactor (PFR) system was used to test both porous inserts. The PFR was configured in a single-zone furnace as the heat transfer chamber. The reactor system included a steam generator placed directly prior to

the reactor inlet, a PFR housed within the furnace, and a condenser located at the reactor outlet. The porous insert was packed in a 7 mm ID quartz tube, which was necked at the center.

5 The feed water was fed to the steam generator using a Cole Parmer syringe pump. Carbon monoxide and nitrogen (a diluent) were fed to the system using Matheson mass flow controllers. The mixed feed stream flowed through the steam generator before entering the PFR in a downflow fashion. The product gases were directed through the condenser and sent to an on-line gas chromatograph, where the product stream was analyzed.

10 Two thermocouples were placed inside the catalytic PFR system. One thermocouple was located above the porous insert. The second thermocouple was placed adjacent to the porous insert outside of the quartz tube to measure the furnace temperature. A pressure gauge at the reactor inlet was used to measure the differential pressure across the porous insert.

15 The product gases were analyzed immediately upon exit from the reactor with a Microsensor Technology Inc., (MTI) M200 Gas Chromatograph. Using a 10-m molecular sieve column (argon carrier gas, 100 °C, 34.1 psig) and an 8-m PoraplotU column (helium carrier gas, 65 °C, 26.9 psig) in parallel, the GC analyzes for hydrogen, nitrogen, oxygen, methane, carbon monoxide, air, carbon dioxide, ethane, and ethylene in 75 sec. The M200 used a vacuum pump to draw a small sample from the product stream with a 40-sec purge and a 100-millisecond injection time. Water was removed from the gas stream prior to entering the M200.

20 Carbon monoxide conversion was calculated based on the moles of material in the inlet and outlet gas stream, as shown in equation 1. The selectivity to carbon dioxide (and hydrogen) or methane was calculated in equations 2 and 3, respectively.

$$X_{CO} = 100 * (n_{CO-in} - n_{CO-out}) / n_{CO-in} \quad (1)$$

$$S_{CO_2} = 100 * n_{CO_2} / (n_{CO_2} + n_{CH_4}) \quad (2)$$

30 $S_{CH_4} = 100 - S_{CO_2} \quad (3)$

Using the first porous insert, fine catalyst powders (65 to 100 mesh), the intrinsic reaction kinetics were approximately measured. The contact time varied from 10 milliseconds to 1 sec. FIG.'s 2a and 2b show the performance for long

and short contact times. At 300 °C and a steam to carbon ratio of 3:1, 25 milliseconds on the Ru-based catalyst was sufficient to convert greater than 98% of the carbon monoxide to carbon dioxide and hydrogen. At 50 milliseconds, a CO conversion of 99.8 % was measured with a selectivity of 100% to the desired products (CO₂ and H₂). The equilibrium conversion of CO at 300 °C and a steam to carbon ratio of 3:1 was 99.93%.

Tests run with longer contact times (> 100 milliseconds) showed the formation of methane, which has an equilibrium selectivity of 22.82%. The equilibrium selectivity line for carbon dioxide and hydrogen is shown on FIG. 2a.

10 As the contact time increased, the formation of methane also increased. A software package, FACT™, was used for all equilibrium calculations.

The results with the second porous insert (coated metal foam) are shown in FIG. 3. At 300 °C, the CO conversion was less than 10%. However, at 500 °C and a steam to carbon ratio of 3:1, the measured carbon monoxide conversion reached 94% with a contact time of 50 milliseconds. The equilibrium conversion was 94.53% at these conditions. With a contact time as short as 10 milliseconds, the carbon monoxide conversion exceeded 90% and 100% selectivity to carbon dioxide and hydrogen was observed. The equilibrium CO₂ selectivity was 93.52% at 500 °C.

20 At the contact times of 10, 50, and 100 milliseconds, the measured selectivity remained near 100%, with methane below the detectability limit of the GC. These findings showed that desired non-equilibrium chemistry was exploited in the coated metal foam. Unwanted series and slow parallel reaction pathways, such as the formation of methane, were effectively shut down.

25 The second porous insert of the coated metal foam had a higher activation temperature than the first porous insert of catalyst powder for two reasons. First, the catalyst washcoat had a slightly different composition and structure than the catalyst powders. Independent catalyst tests with powders made from the same washcoat verified the higher required activation temperature. The other 30 distinction between the two porous inserts was a reduced weight of active catalyst (approximately 10%) on the coated metal foam.

Example 2

An experiment was conducted to demonstrate hydrocarbon steam reforming according to the present invention.

Using the first porous insert (powder) as in Example 1, methane steam reforming was achieved with 100% conversion at 850 °C in 25 milliseconds on a 5%Rh/ γ -Al₂O₃ catalyst (FIG. 4). Using the second porous insert (coated metal foam) as in Example 1, with a 5%Rh/ γ -Al₂O₃ catalyst/interfacial layers on 80 ppi stainless steel metal foam reduced the operating temperature by 100 °C to achieve the same performance at 750 °C.

No coke formation was observed during any of the millisecond residence time experiments with lower steam to methane ratios (2.5:1).

Results for other hydrocarbons are shown in Table E2-1 wherein "time" is residence time.

Table E2-1: Preliminary hydrocarbon reforming data based on 5%Rh/ γ -Al₂O₃ catalyst screening tests

Hydrocarbon	Temperature (C)	Time (ms)	Conversion %	H2 Sel. %
Butane	600	25	100	96
Gasoline	800	50	95	~ 95
Iso-octane ^A	700	25	100	89.5
Kerosene	600	50	95	~ 98

^A Catalyst material included a titania buffer layer

Further data for an n-butane steam reforming experiment are shown in FIG. 5a. A porous insert of 80 ppi stainless steel with an interfacial layer of alumina and a catalyst material of rhodium (15.6 wt% Rh on 17.1 wt% alumina, balance stainless steel foam, no buffer layer). Conditions were 650 °C at 95 ms residence time with a steam to carbon ratio of 3.58:1. The pressure drop increased from negligible to over 7 psig, attributed to cracking and spalling of the interfacial and catalyst layers. The catalyst was regenerated in air to remove deposited carbon. FIG. 5b shows poorer performance. Pressure drop increased to over 7 psig after only 5 operating hours in two days.

CLOSURE

While a preferred embodiment of the present invention has been shown and described, it will be apparent to those skilled in the art that many changes and modifications may be made without departing from the invention in its broader aspects. The appended claims are therefore intended to cover all such changes and modifications as fall within the true spirit and scope of the invention.

CLAIMS

5

We claim:

1. A method for obtaining an enhanced production rate per reaction chamber volume of a reaction chamber having an inlet and an outlet for a thermal chemical reaction, the method comprising the steps of:
 - (a) placing a porous insert within said reaction chamber volume, wherein a reactant flow substantially completely passes through said porous insert wherein said reaction chamber volume with said porous insert has a mean porosity less than 1 and a transport distance no greater than 3 mm;
 - (b) sizing said reaction chamber volume with a length parallel to a bulk reactant flow, said length less than or equal to 6 inches, and with a height less than or equal to 2 inches, thereby transferring reaction heat at an enhanced heat transfer rate through said porous insert; and
 - (c) providing a heat transfer chamber in thermal contact with the reaction chamber volume, said heat transfer chamber transferring heat at said enhanced heat transfer rate across a wall between the heat transfer chamber and the reaction chamber, thereby obtaining the enhanced production rate per reaction chamber volume for the thermal chemical reaction wherein a ratio of said enhanced production rate per reaction chamber volume to a conventional production rate per conventional reaction chamber volume for the thermal chemical reaction is at least 2.
2. The method as recited in claim 1, wherein said thermal chemical reaction is a catalytic chemical reaction.
- 30 3. The method as recited in claim 2, wherein a catalyst is on the porous insert.

4. The method as recited in claim 3, wherein said porous insert has a solution deposited interfacial layer thereon, and a catalyst metal on the interfacial layer.

5 5. The method as recited in claim 4, wherein said porous insert has a buffer layer between the porous support and the solution deposited interfacial layer.

10 6. The method as recited in claim 5, wherein said buffer layer is a metal oxide.

7. The method as recited in claim 6, wherein said metal oxide is selected from the group consisting of Al_2O_3 , TiO_2 and combinations thereof.

15 8. The method as recited in claim 7, wherein said Al_2O_3 is selected from the group consisting of $\alpha\text{-Al}_2\text{O}_3$, $\gamma\text{-Al}_2\text{O}_3$ and combinations thereof.

20 9. A method of obtaining an enhanced production rate per reaction chamber volume of a reaction chamber having an inlet and an outlet for a steam reforming thermal chemical reaction, the method comprising the steps of;

25 (a) placing a porous insert within said reaction chamber volume, wherein a reactant flow substantially completely passes through said porous insert wherein said reaction chamber volume with said porous insert has a mean porosity less than 1 and a transport distance no greater than 3 mm, said porous insert comprising a porous support with a catalyst material thereon;

(b) sizing said reaction chamber volume with a length parallel to a bulk reactant flow, said length less than or equal to 6 inches, and with a height less than or equal to 2 inches, thereby transferring reaction heat at an enhanced heat transfer rate through said porous insert; and

30 (c) providing a heat transfer chamber in thermal contact with the reaction chamber volume, said heat transfer chamber transferring heat at said enhanced heat transfer rate across a wall between the heat transfer chamber and the reaction chamber, thereby obtaining the enhanced production rate per

reaction chamber volume for the thermal chemical reaction wherein a ratio of said enhanced production rate per reaction chamber volume to a conventional production rate per conventional reaction chamber volume for the thermal chemical reaction is at least 2.

5

10. The method as recited in claim 9, wherein said porous insert further has an interfacial layer between said porous support and said catalyst material.

11. The method as recited in claim 10, wherein said porous insert
10 further has a buffer layer between said interfacial layer and said porous support.

12. A method of obtaining an enhanced production rate per reaction chamber volume of a reaction chamber having an inlet and an outlet for a water gas shift thermal chemical reaction, the method comprising the steps of;

15 (a) placing a porous insert within said reaction chamber volume, wherein a reactant flow substantially completely passes through said porous insert wherein said reaction chamber volume with said porous insert has a mean porosity less than 1 and a transport distance no greater than 3 mm, said porous insert comprising a porous support with a catalyst material thereon;

20 (b) sizing said reaction chamber volume with a length parallel to a bulk reactant flow, said length less than or equal to 6 inches, and with a height less than or equal to 2 inches, thereby transferring reaction heat at an enhanced heat transfer rate through said porous insert; and

25 (c) providing a heat transfer chamber in thermal contact with the reaction chamber volume, said heat transfer chamber transferring heat at said enhanced heat transfer rate across a wall between the heat transfer chamber and the reaction chamber, thereby obtaining the enhanced production rate per reaction chamber volume for the thermal chemical reaction wherein a ratio of said enhanced production rate per reaction chamber volume to a conventional production rate per conventional reaction chamber volume for the thermal chemical reaction is at least 2.

13. A vessel for obtaining an enhanced production rate per reaction chamber volume of a reaction chamber having an inlet and an outlet for a thermal chemical reaction, the vessel comprising;

- (a) a porous insert within said reaction chamber volume,
5 wherein a reactant flow substantially completely passes through said porous insert wherein said reaction chamber volume with said porous insert has a mean porosity less than 1 and a transport distance no greater than 3 mm;
- (b) said reaction chamber volume having a length parallel to a bulk reactant flow, said length less than or equal to 6 inches, and with a height
10 less than or equal to 2 inches, thereby transferring reaction heat at an enhanced heat transfer rate through said porous insert; and
- (c) a heat transfer chamber in thermal contact with the reaction chamber volume, said heat transfer chamber transferring heat at said enhanced heat transfer rate across a wall between the heat transfer chamber and the
15 reaction chamber, thereby obtaining the enhanced production rate per reaction chamber volume for the thermal chemical reaction wherein a ratio of said enhanced production rate per reaction chamber volume to a conventional production rate per conventional reaction chamber volume for the thermal chemical reaction is at least 2.

20

14. The vessel as recited in claim 13, wherein said thermal chemical reaction is a catalytic chemical reaction.

25

15. The vessel as recited in claim 14, wherein a catalyst material is on the porous insert.

16. The vessel as recited in claim 14, wherein said porous insert has a solution deposited interfacial layer between a porous support and the catalyst material.

30

17. The vessel as recited in claim 16, wherein said porous insert has a solution deposited interfacial layer between said porous support and said catalyst material.

18. The vessel as recited in claim 17, wherein said porous insert has a buffer layer between the porous support and the solution deposited interfacial layer.

5

19. The vessel as recited in claim 18, wherein said buffer layer is a metal oxide.

10 20. The vessel as recited in claim 19, wherein said metal oxide is selected from the group consisting of Al_2O_3 , TiO_2 and combinations thereof.

21. The vessel as recited in claim 19, wherein said Al_2O_3 is selected from the group consisting of $\alpha\text{-Al}_2\text{O}_3$, $\gamma\text{-Al}_2\text{O}_3$ and combinations thereof.

15 22. The vessel as recited in claim 16, wherein said porous support is a metal foam.

23. The vessel as recited in claim 16, wherein said porous support is a porous ceramic.

20

24. The vessel as recited in claim 17, wherein said interfacial layer is a solution deposited metal oxide.

25 25. The vessel as recited in claim 24, wherein said solution deposited metal oxide is selected from the group consisting of $\gamma\text{Al}_2\text{O}_3$, SiO_2 , ZrO_2 , TiO_2 and combinations thereof.

30 26. The vessel as recited in claim 15, wherein said catalyst material is a metal selected from the group of noble metal, transition metal and combinations thereof.

27. The vessel as recited in claim 13, wherein said buffer layer is a vapor deposited metal oxide.

28. The vessel as recited in claim 27, wherein said vapor deposited metal oxide is selected from the group of Al_2O_3 , TiO_2 and combinations thereof.

29. The vessel as recited in claim 27, wherein said Al_2O_3 is selected
5 from the group consisting of $\alpha\text{-Al}_2\text{O}_3$, $\gamma\text{-Al}_2\text{O}_3$ and combinations thereof.

30. The vessel as recited in claim 13 wherein said buffer layer comprises a plurality of sublayers.

1/3

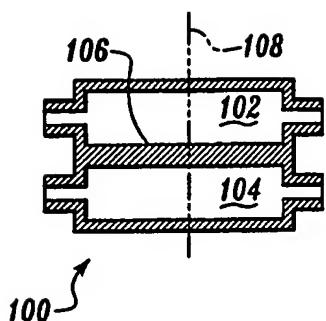


Fig. 1a

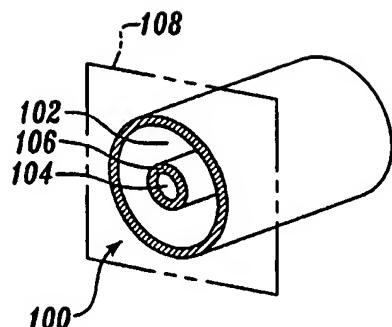


Fig. 1b

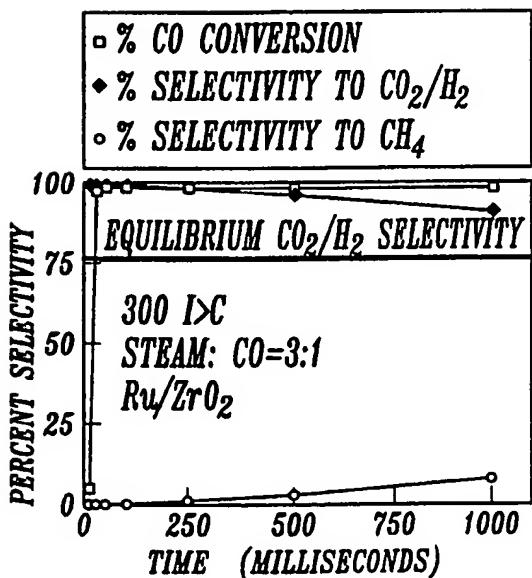


Fig. 2a

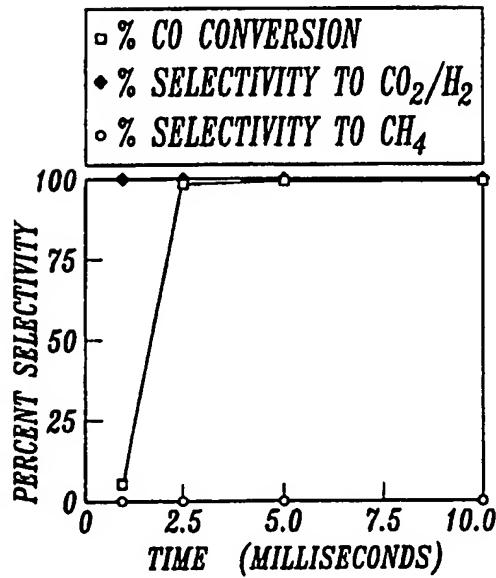


Fig. 2b

2/3

CONVERSION AND CO SELECTIVITY VS. TEMPERATURE
FOR %Ru/ZrO₂/Ni AT 10, 50 AND 100 mSEC RESIDENCE
TIME, 3:1 STEAM:CO, 5% CO IN FEED

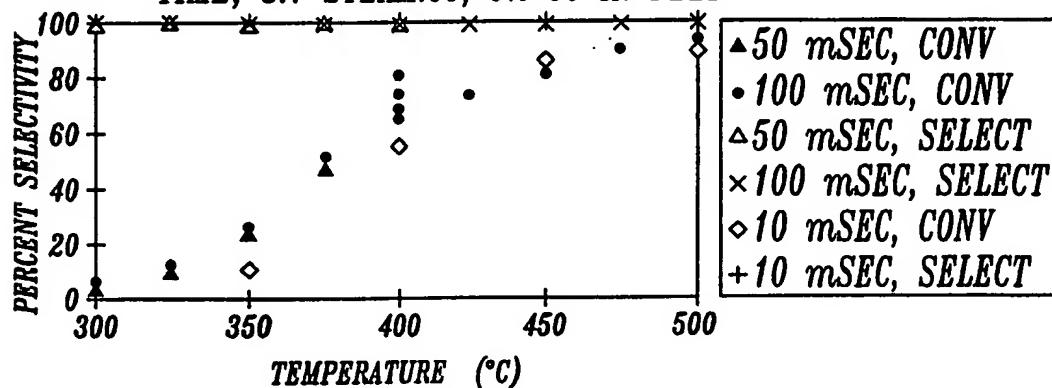


Fig. 3

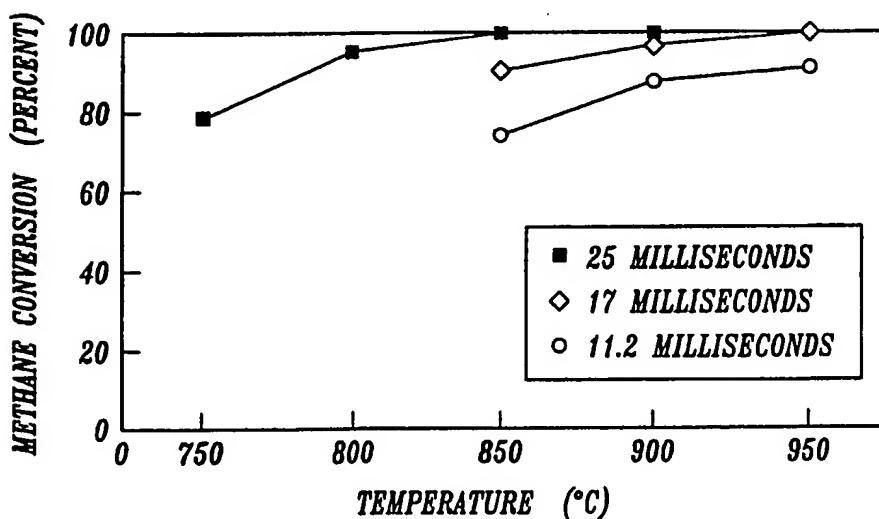


Fig. 4

3/3

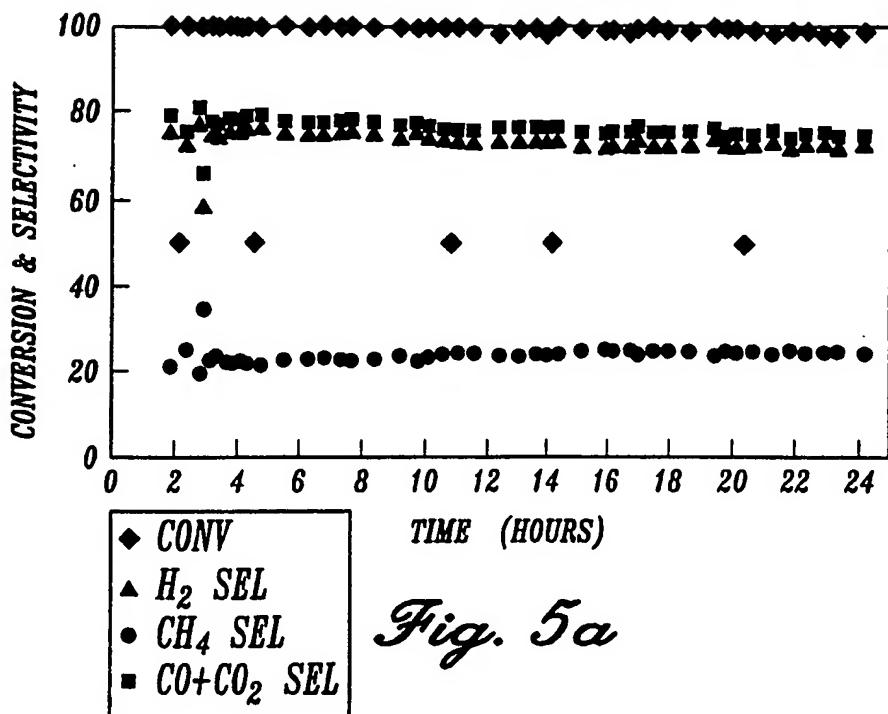


Fig. 5a

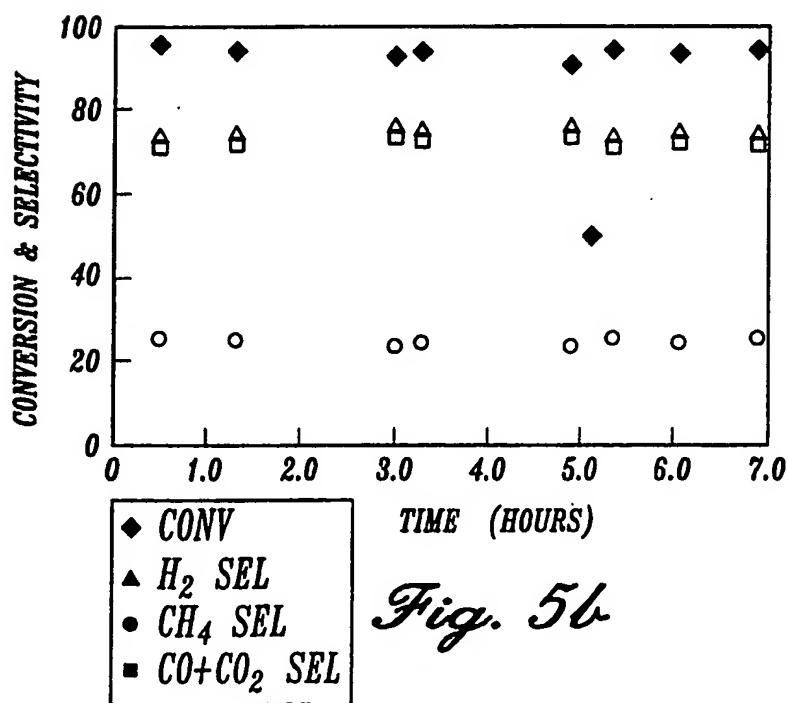


Fig. 5b

INTERNATIONAL SEARCH REPORT

International Application No
PCT/US 99/17084

A. CLASSIFICATION OF SUBJECT MATTER
 IPC 7 B01J8/02 C01B3/38 C01B3/16 B01J12/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01J C01B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the International search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	WO 96 32188 A (GASTEC NV ;WAL WILLEM JOHAN JACOB V D (NL); WINGERDEN ANTONIUS JOH) 17 October 1996 (1996-10-17) page 13, line 27 -page 16, line 10 page 17, line 13 -page 19, line 9 page 21, line 26 -page 22, line 3 claims 1-14; figures 1,2 -----	1-3, 9, 12-15
A	US 4 795 618 A (LAUMEN MICHAEL) 3 January 1989 (1989-01-03) column 5, line 50 -column 6, line 39 claims 1-5; figures 1,2,4 -----	1-3, 13-15
A	WO 97 39490 A (ZTEK CORP) 23 October 1997 (1997-10-23) claims 1-79; figures 1,2 -----	9, 12

Further documents are listed in the continuation of box C.

Patent family members are listed in annex.

* Special categories of cited documents :

- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier document but published on or after the International filing date
- "L" document which may throw doubt on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the International filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

Date of the actual completion of the International search

12 November 1999

Date of mailing of the International search report

22/11/1999

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo rd.
Fax: (+31-70) 340-3016

Authorized officer

Vlassis, M

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/US 99/17084

Patent document cited in search report	Publication date	Patent family member(s)			Publication date
WO 9632188	A 17-10-1996	NL	1000146 C		15-10-1996
		AU	5164196 A		30-10-1996
		EP	0869842 A		14-10-1998
		JP	11504563 T		27-04-1999
-----	-----	-----	-----	-----	-----
US 4795618	A 03-01-1989	DE	3435319 A		03-04-1986
		AU	4951585 A		17-04-1986
		WO	8602016 A		10-04-1986
		EP	0197108 A		15-10-1986
		JP	62500438 T		26-02-1987
-----	-----	-----	-----	-----	-----
WO 9739490	A 23-10-1997	US	5858314 A		12-01-1999
		AU	2545597 A		07-11-1997
		CA	2251627 A		23-10-1997
		CZ	9803240 A		14-04-1999
		EP	0904608 A		31-03-1999
		NO	984721 A		07-12-1998
		PL	329316 A		15-03-1999
-----	-----	-----	-----	-----	-----